

**Czech Hydrogen Days**

**Praha, 18 to 20 March 2015**



**UNIVERSITY OF  
BIRMINGHAM**

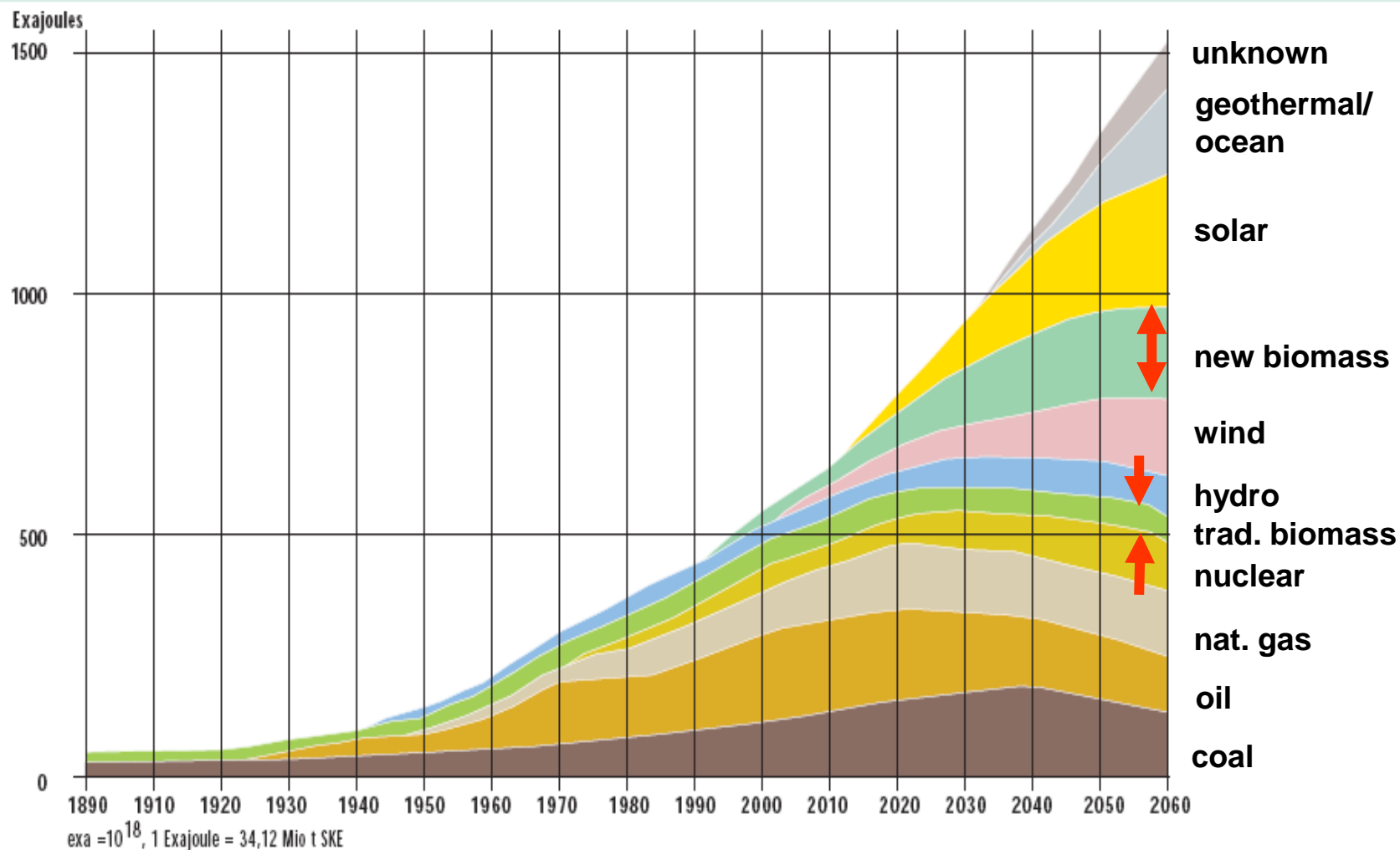
# **Hydrogen from Biomass – A Complex Process**

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University of Birmingham



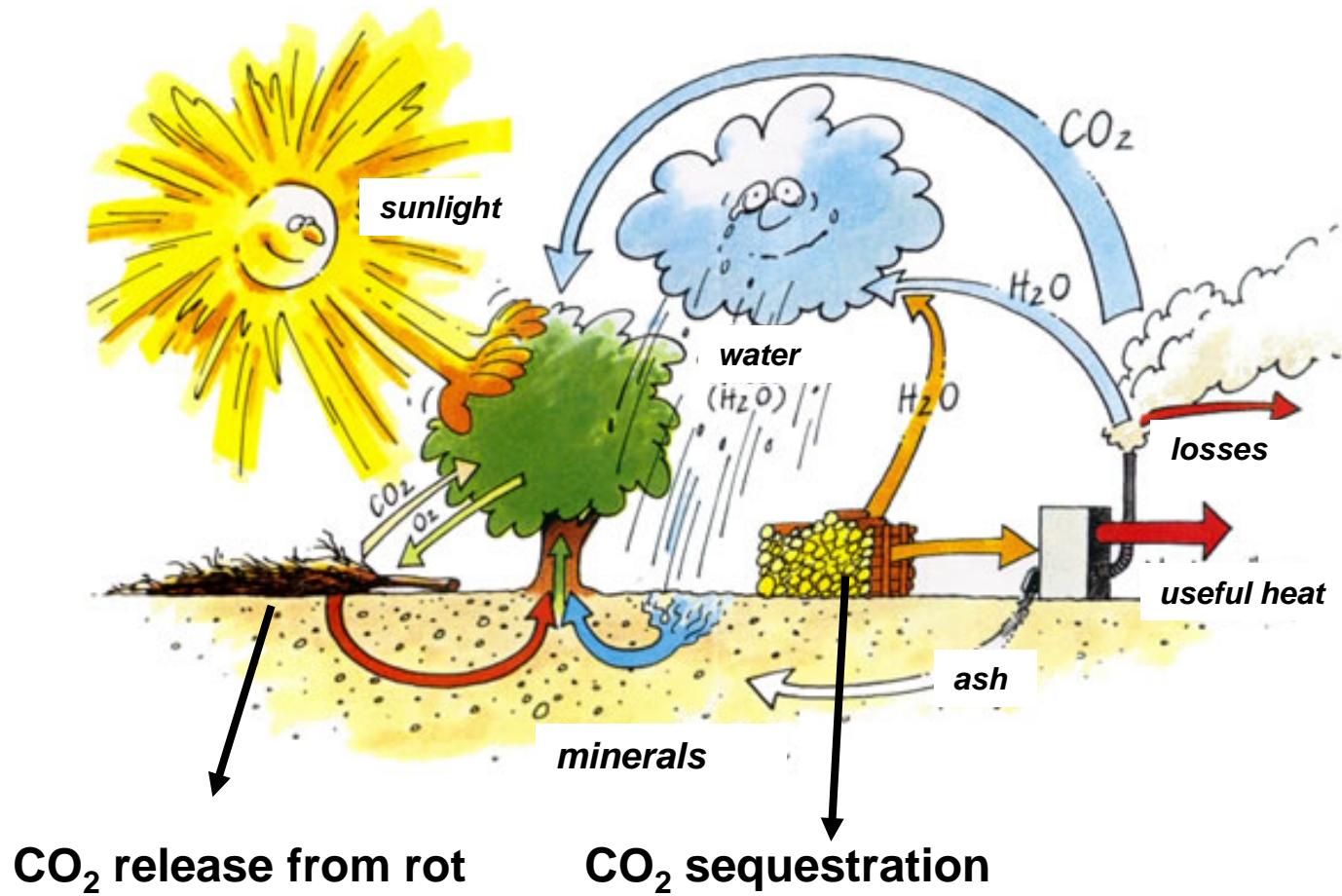


# Shell World Energy Scenario (‘thinkable’ development)



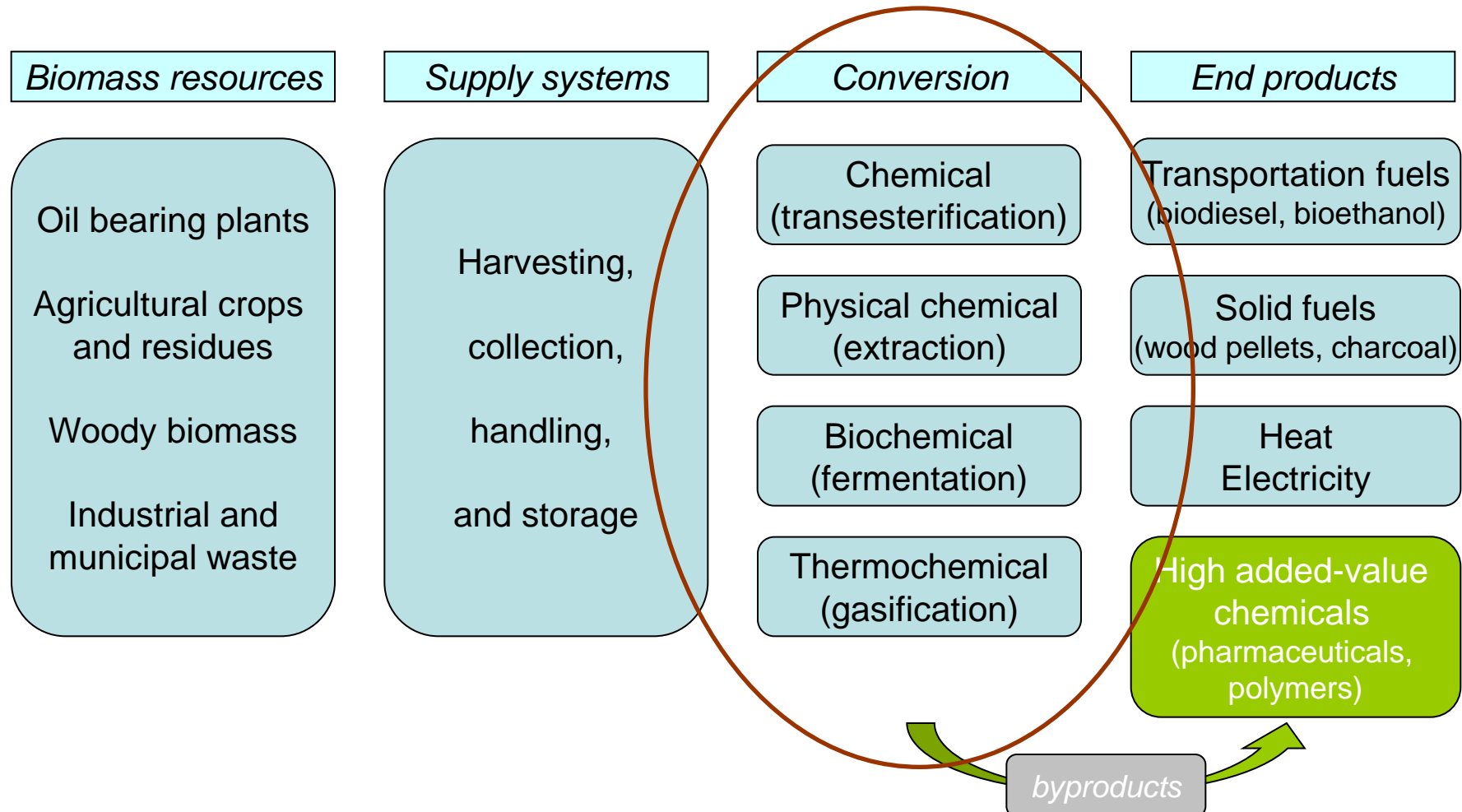
Source: Deutsche  
Shell, 1999

# Natural CO<sub>2</sub> Recycling



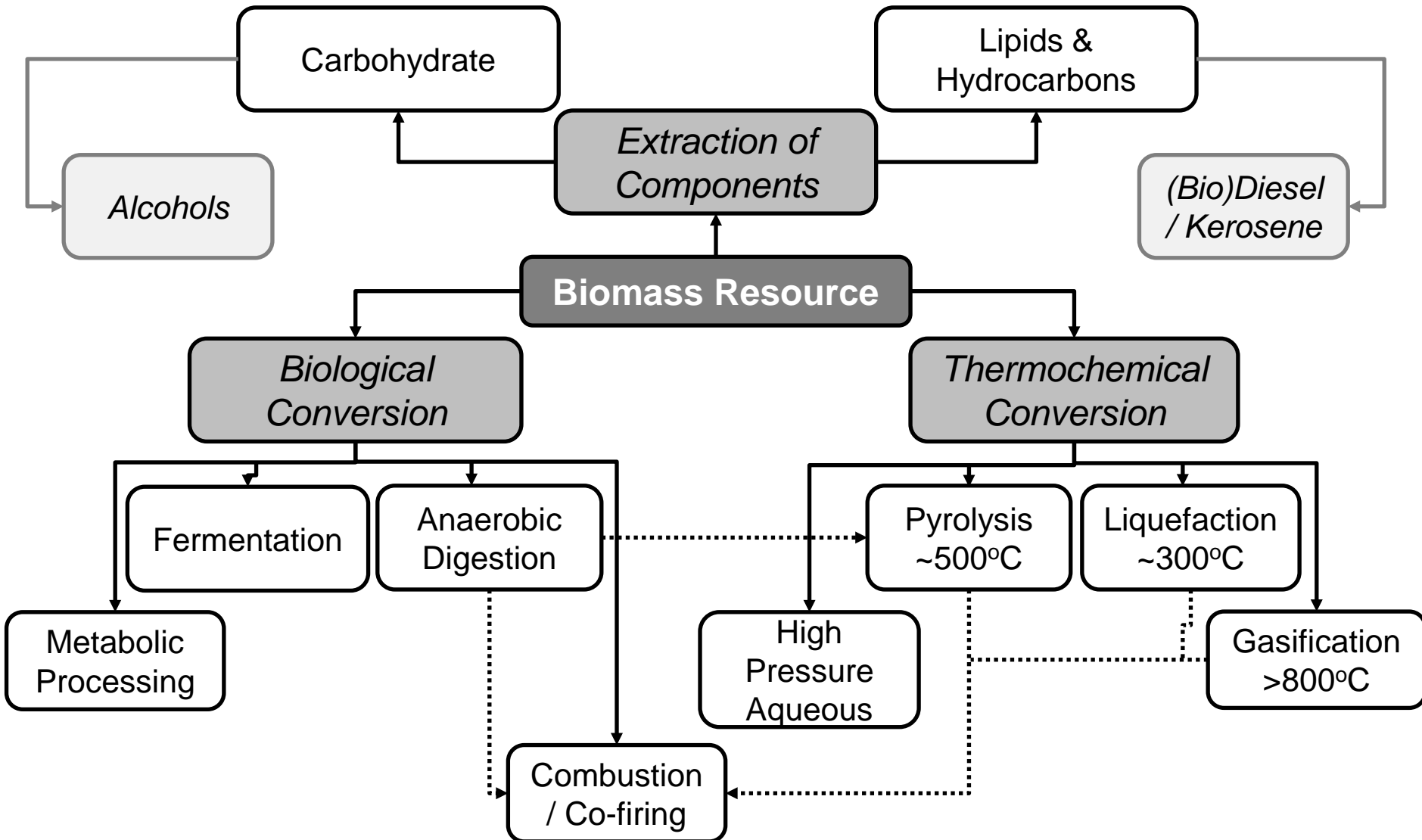
Graphics courtesy MW BaWü

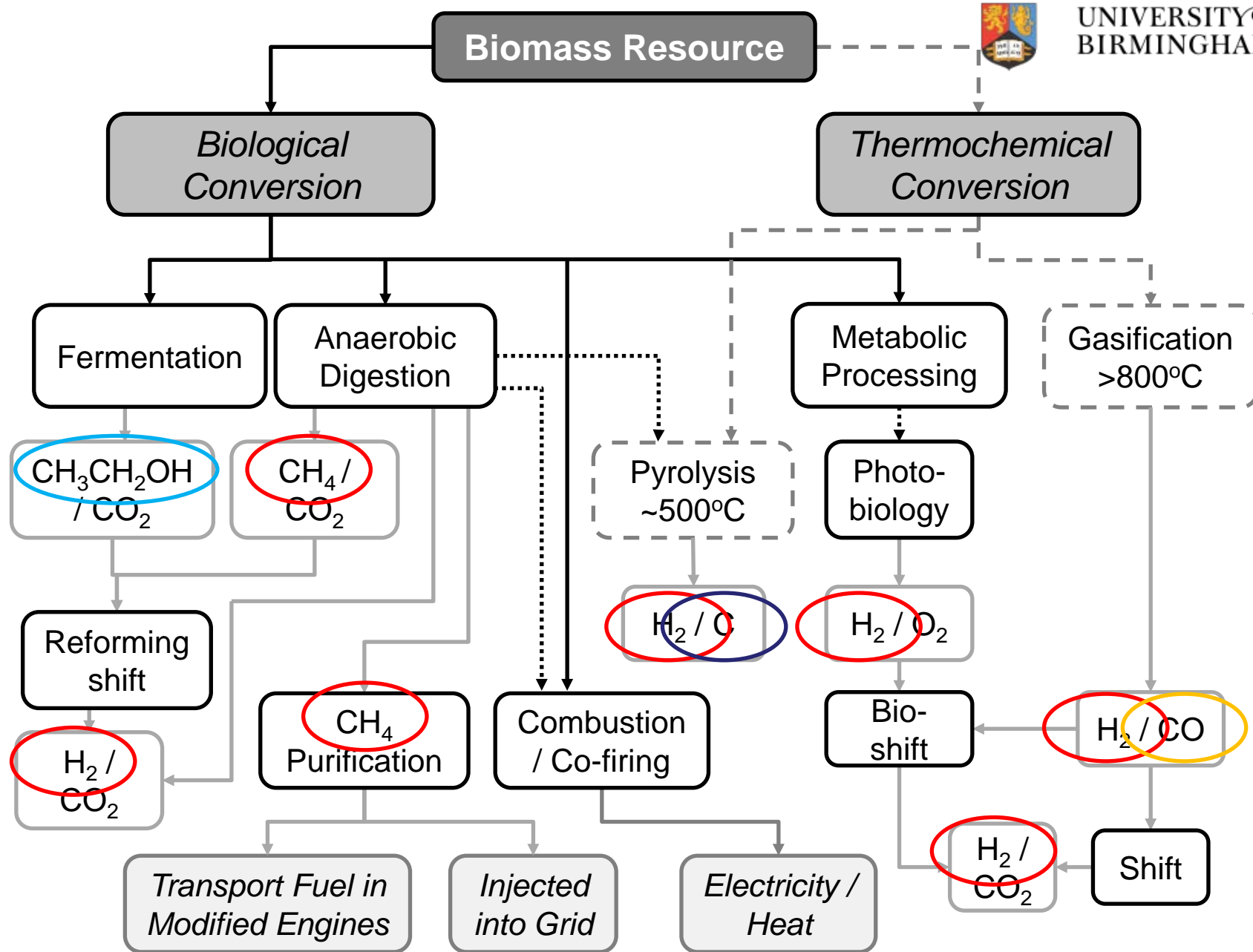
# Biomass chain





# Biomass Conversion Pathways





# Fuel Processing – Reactions

## Steam reforming

- $C_xH_yO_z + (x-z) H_2O \rightarrow x CO + (x-z+y/2) H_2$
- $CH_4 + H_2O \leftrightarrow CO + 3 H_2$

## Water gas shift reaction

- $CO + H_2O \leftrightarrow CO_2 + H_2$

## CPO “Catalytic Partial Oxidation”

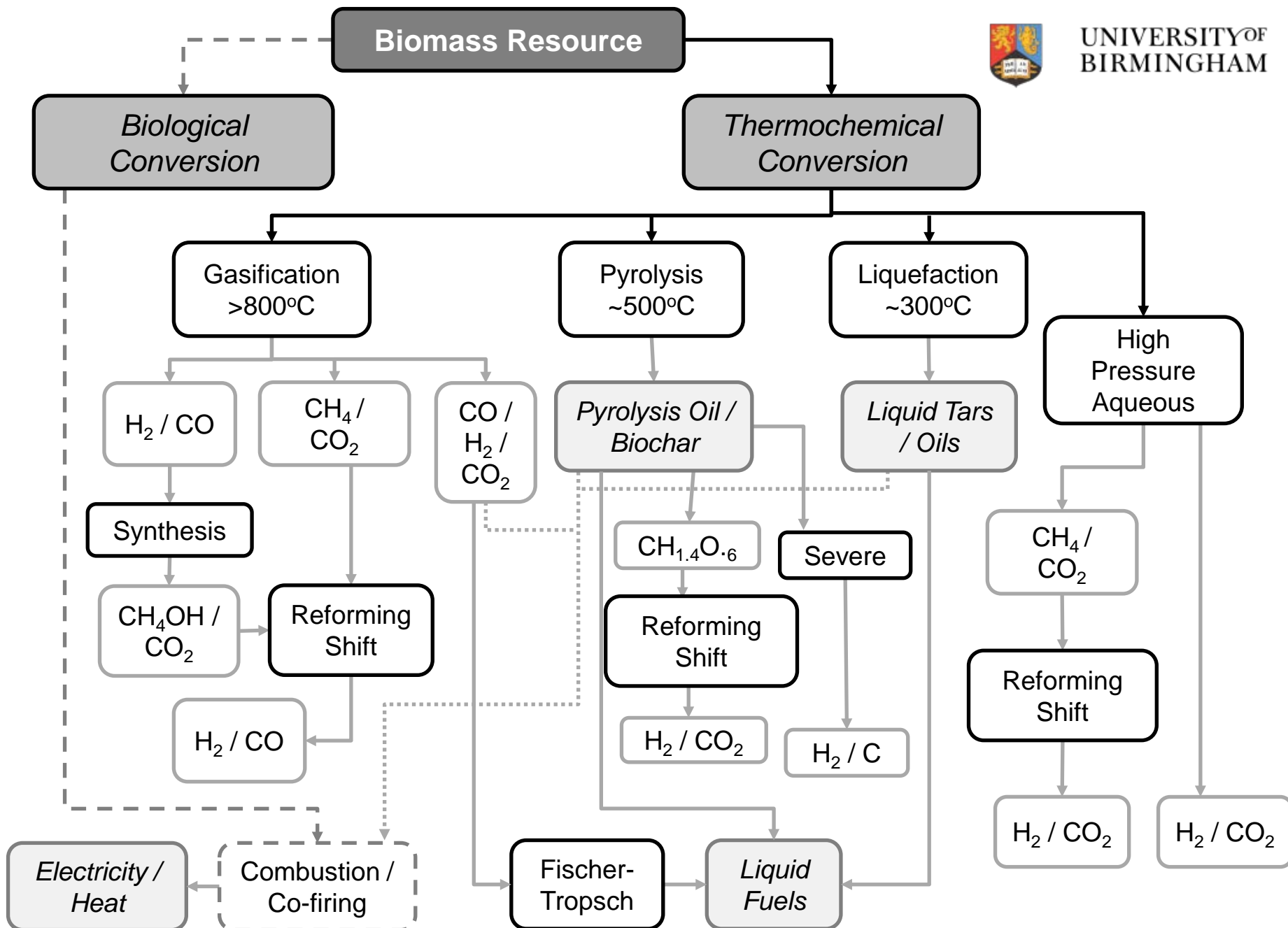
- $C_xH_yO_z + (x-z)/2 (O_2 + 3.76 N_2) \rightarrow x CO + y/2 H_2 + 3.76(x-z)/2 N_2$

## ATR “Autothermal Reforming”

- $C_xH_yO_z + n(O_2 + 3.76 N_2) + (x-2n-z) H_2O \rightarrow x CO + (x-2n-z+y/2) H_2 + 3.76n N_2$

## Dry reforming

- $CH_4 + CO_2 \leftrightarrow 2CO + 2 H_2$

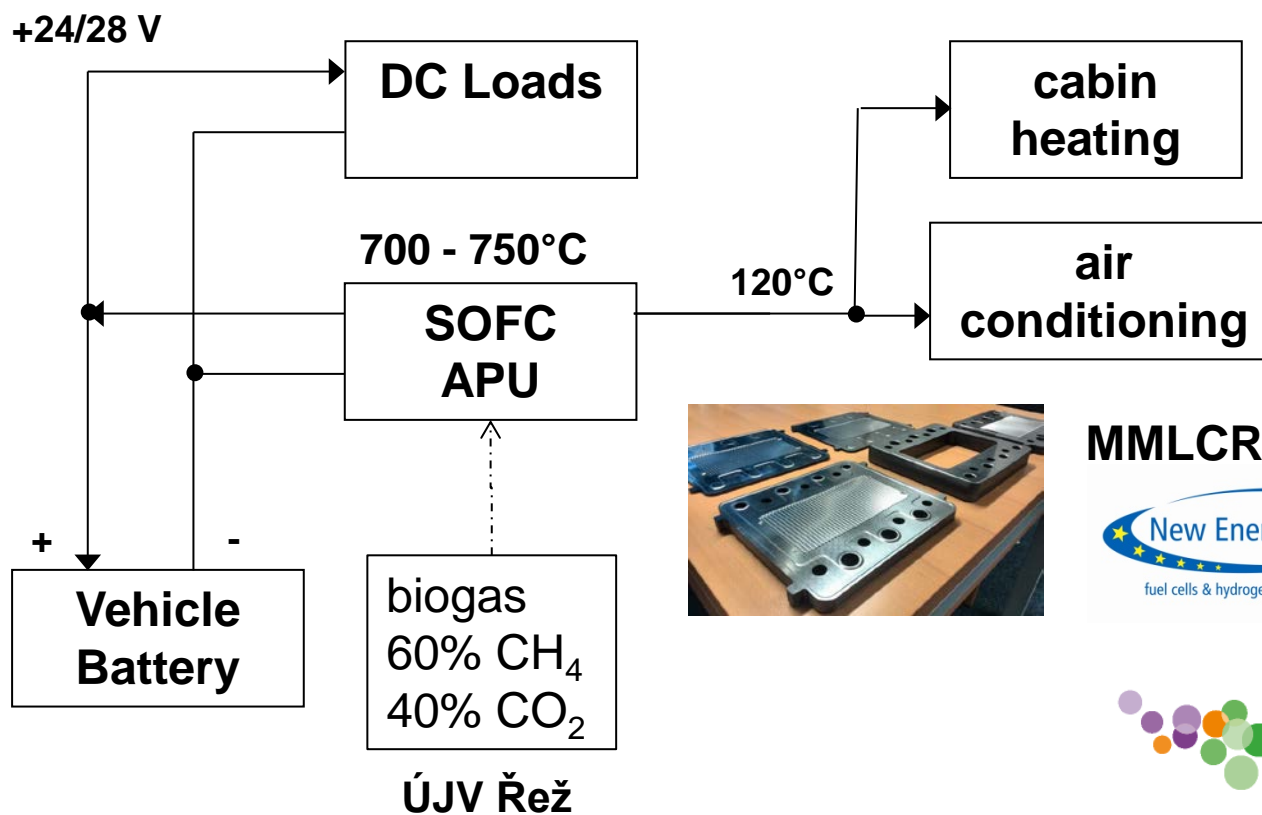




## Fuel Cell Fuel Purity Requirements

| Type | CO      | CO <sub>2</sub> | N <sub>2</sub> | H <sub>2</sub> S | Cl        | particles            |
|------|---------|-----------------|----------------|------------------|-----------|----------------------|
| PEFC | <10 ppm | tol.            | tol.           | 0                | <0,05 ppm | 0                    |
| PAFC | <2%     | tol.            | <2%            | <50 ppm          | <1 ppm    | <1 mg/m <sup>3</sup> |
| MCFC | tol.    | tol.            | tol.           | <0,1 ppm         | <1 ppm    | <1 μm                |
| SOFC | tol.    | tol.            | tol.           | <1 ppm           | <1 ppm    | <1 mg/m <sup>3</sup> |

# Use of Biogas with an SOFC APU



- ▶ no gas processing
- ▶ high electrical efficiency >50%

**MMLCR=SOFC**[www.balticbiogasbus.eu](http://www.balticbiogasbus.eu)

# Methane from Renewable Energy Sources

Realistic sources:

- fermenter gas
- sewage gas
- landfill gas
- mine gas

at development stage:

- gasification of biomass
- gasification of household wastes

new 'hype':

- methane synthesis (power to gas)

# Anaerobic digestion

In absence of air converts animal or plant waste into methane

- Typical Wastes
  - Manure (feed lots, pig farms, poultry)
  - Olive oil mill waste
  - Potato processing waste
- Typical Products
  - Biogas ( $\text{CH}_4$ ,  $\text{CO}_2$ )
  - Fibre or digestate (solid residue similar to compost)
  - Fertilizer (liquid fraction)

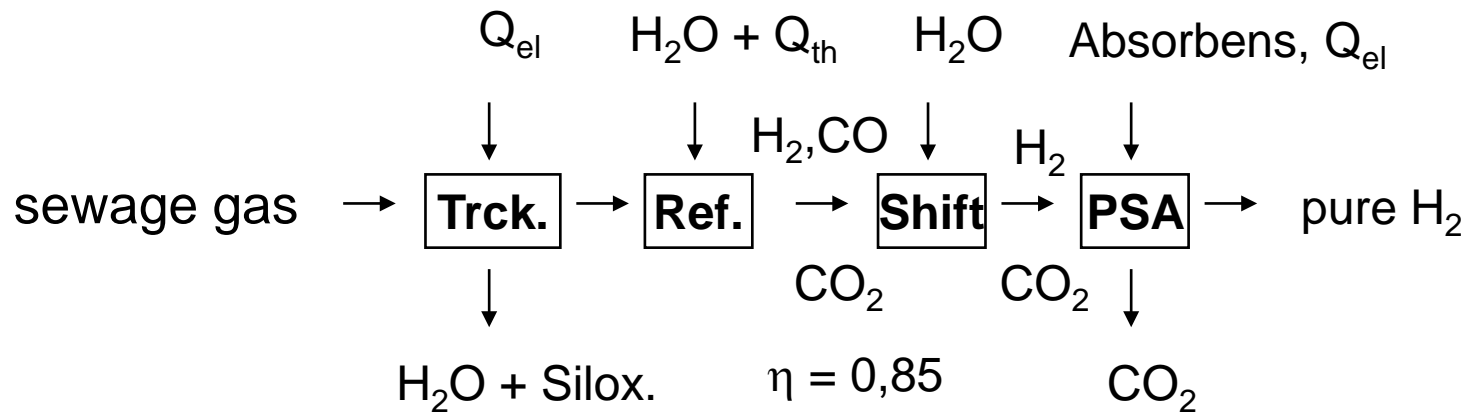


# Gases from Biomass Digestion

| Typ           | CO | CO <sub>2</sub> | N <sub>2</sub> | H <sub>2</sub> S | Cl    | others          | particles |
|---------------|----|-----------------|----------------|------------------|-------|-----------------|-----------|
|               |    |                 |                |                  |       |                 |           |
| Biogas        | 0  | 30 – 40%        | (2%)           | yes              | (yes) | NH <sub>3</sub> | 0         |
| Sewage gas    | 0  | 25 – 35%        | (2%)           | yes              | yes   | Siloxane        | 0         |
| Land fill gas | 0  | 30 – 45%        | 0              | yes              | yes   |                 | 0         |

# Gas Treatment: Sewage Gas - PEFC

*Waste Water Plant Cologne*



problems:

- many process steps with possibility of failure
- high energy demand for PSA

# Carbon Formation Reactions

carbon build-up due to hydrogen and oxygen mismatch

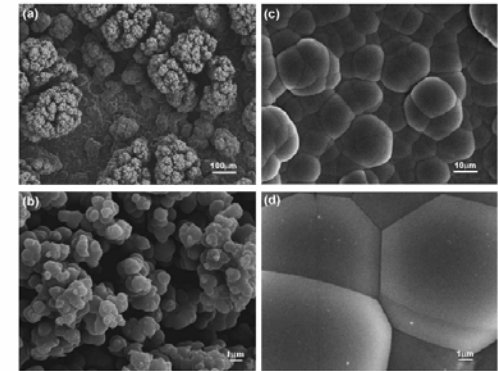
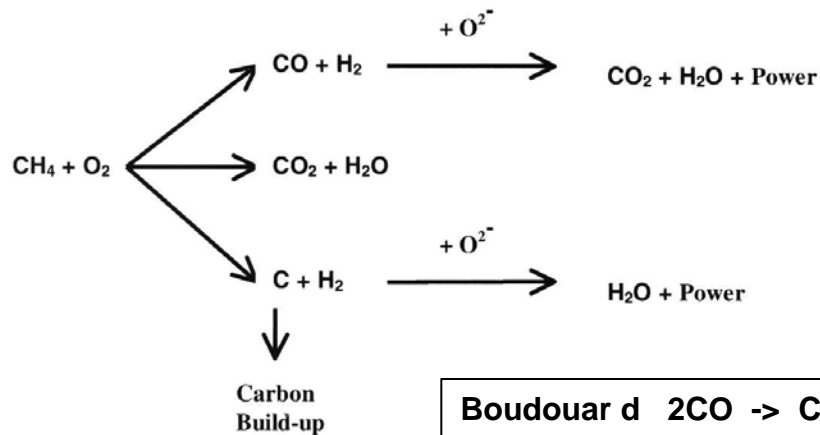
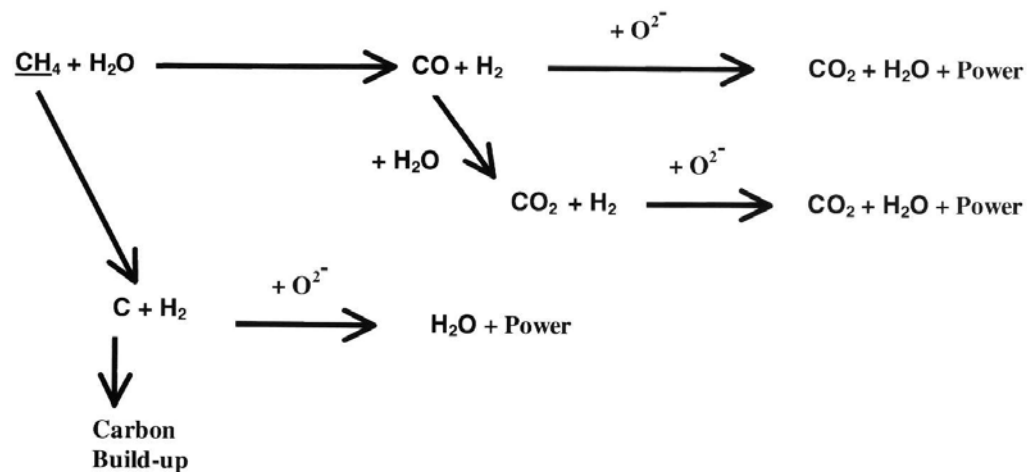
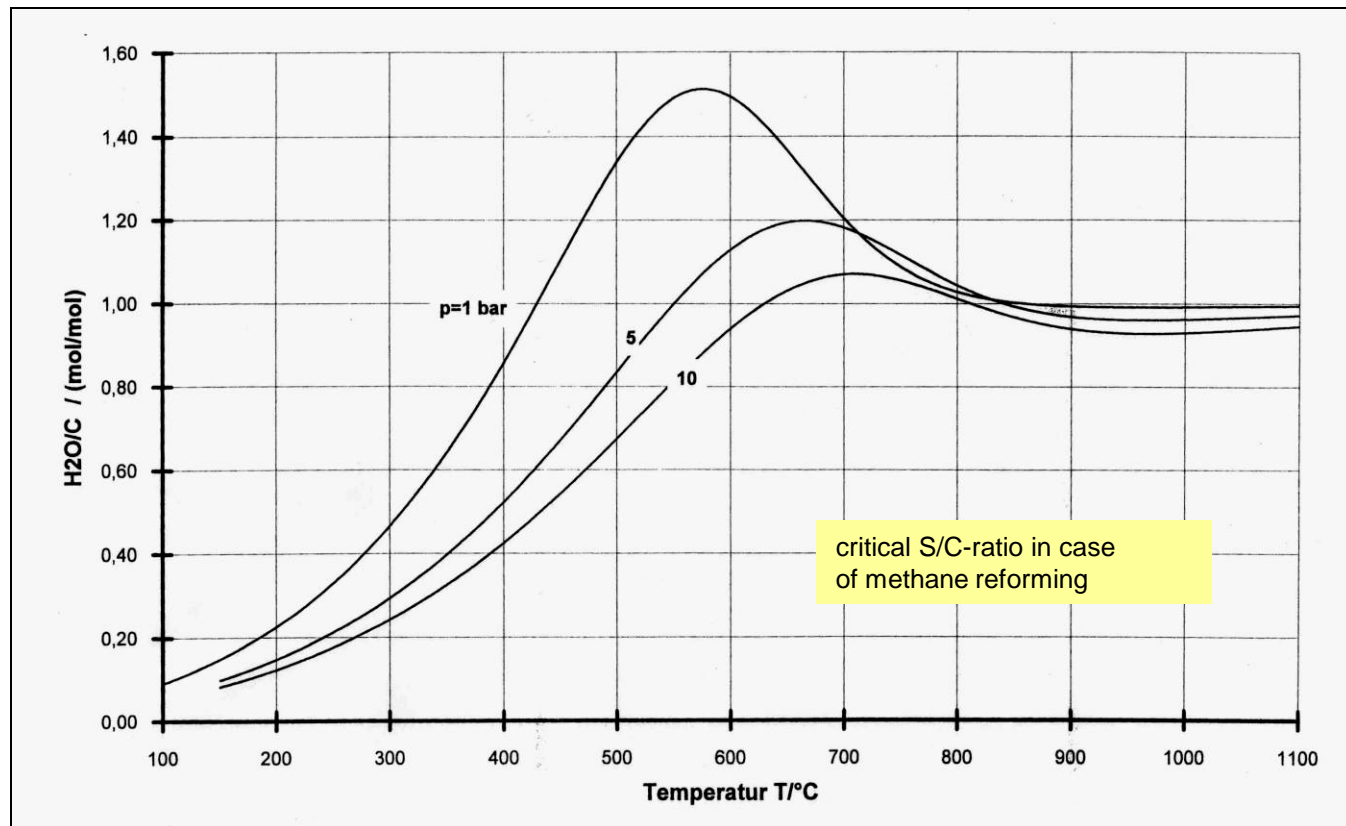


Fig. 4. The morphology of carbonaceous deposits on the surface of an anode containing 10 wt %  $\text{CrO}_2$  and 20 wt % Cu after long-term testing in n-butane at 1173 K.



# Methane Reforming: Carbon formation

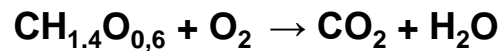
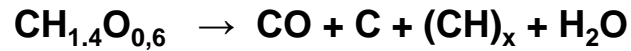


Elemental carbon can develop at and below the curves indicated. Technically the steam-to-carbon ratio is therefore generally chosen as 2,5 to 3 [mol/mol].

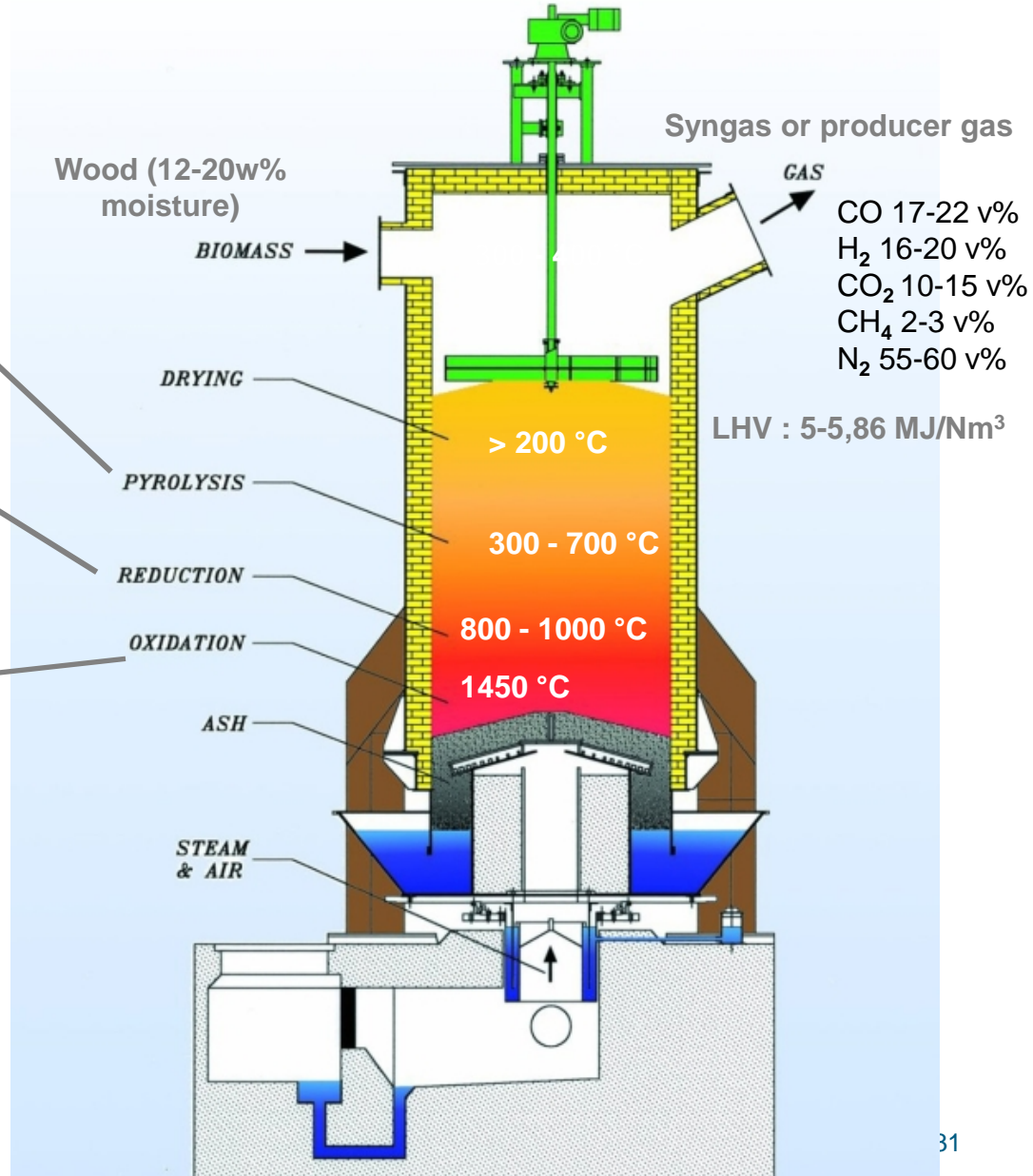
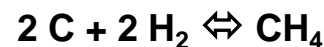
source: A. Gubner



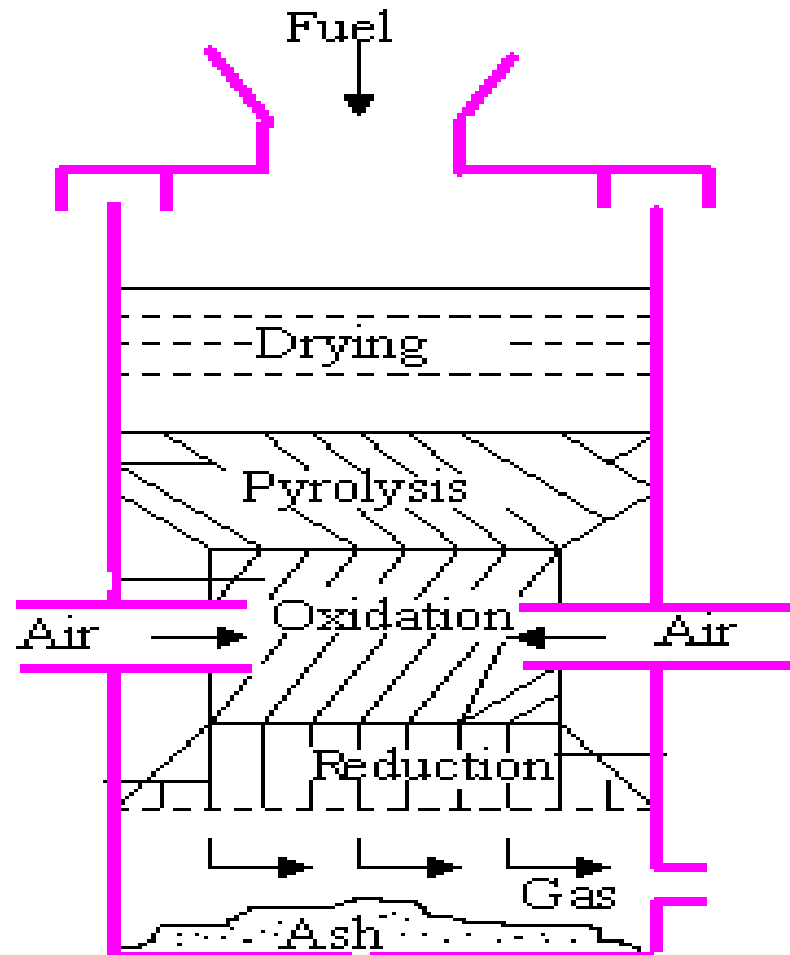
# Updraft Gasifier



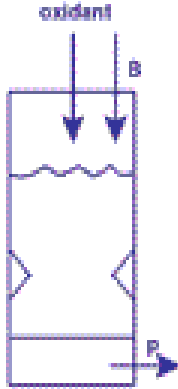
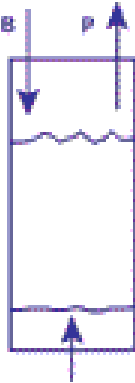
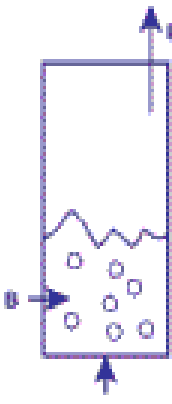
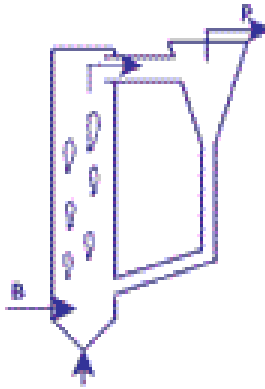
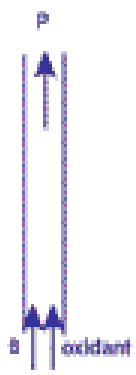
The methane concentration can be increased by pressure increase



# Downdraft Gasifier



# Biomass Gasification: Gasifier types

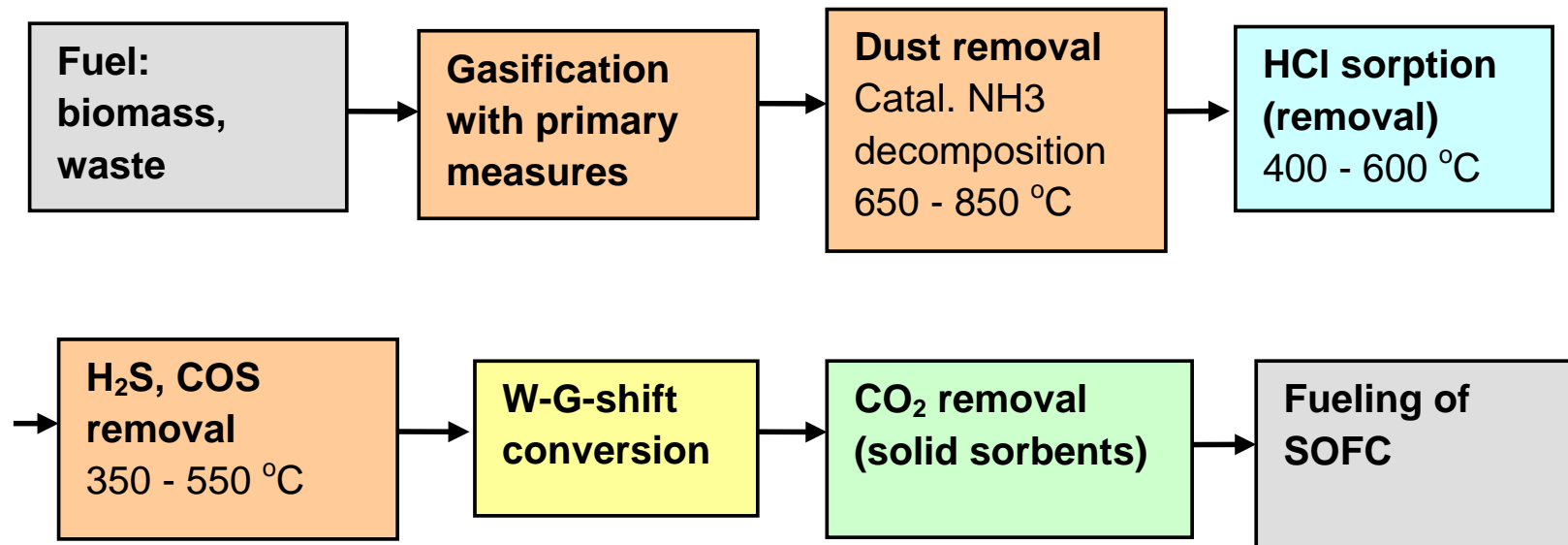
|           |   |                     |  |                       |   |
|-----------|---|---------------------|--|-----------------------|---|
|           |   |                     |   |                       |  |
|           | <div> <div>Mov</div> <div>fixed</div> <div>s</div> </div>   |                     | <div>Fluid beds</div>  |                       | <div>Entrained beds</div>   |
|           | Co-current  | Counter current     | dense  | circulating           |   |
| T°C       | 700-1200  | 700-900             | < 900  | < 900                 | ~1500   |
| tars      | low   | very high           | intermediate   | intermediate          | absent  |
| control   | easy  | very easy           | intermediate   | intermediate          | very complex  |
| scale     | < 5 MW <sub>t</sub>   | < 20 M <sub>t</sub> | 10<MW <sub>t</sub> <100  | 20<MW <sub>t</sub> <? | > 100 MW <sub>t</sub>   |
| feedstock | very critical   | critical            | less critical  | less critical         | very fine particles   |

source: BTG

## Biomass Gasification: Product gas quality

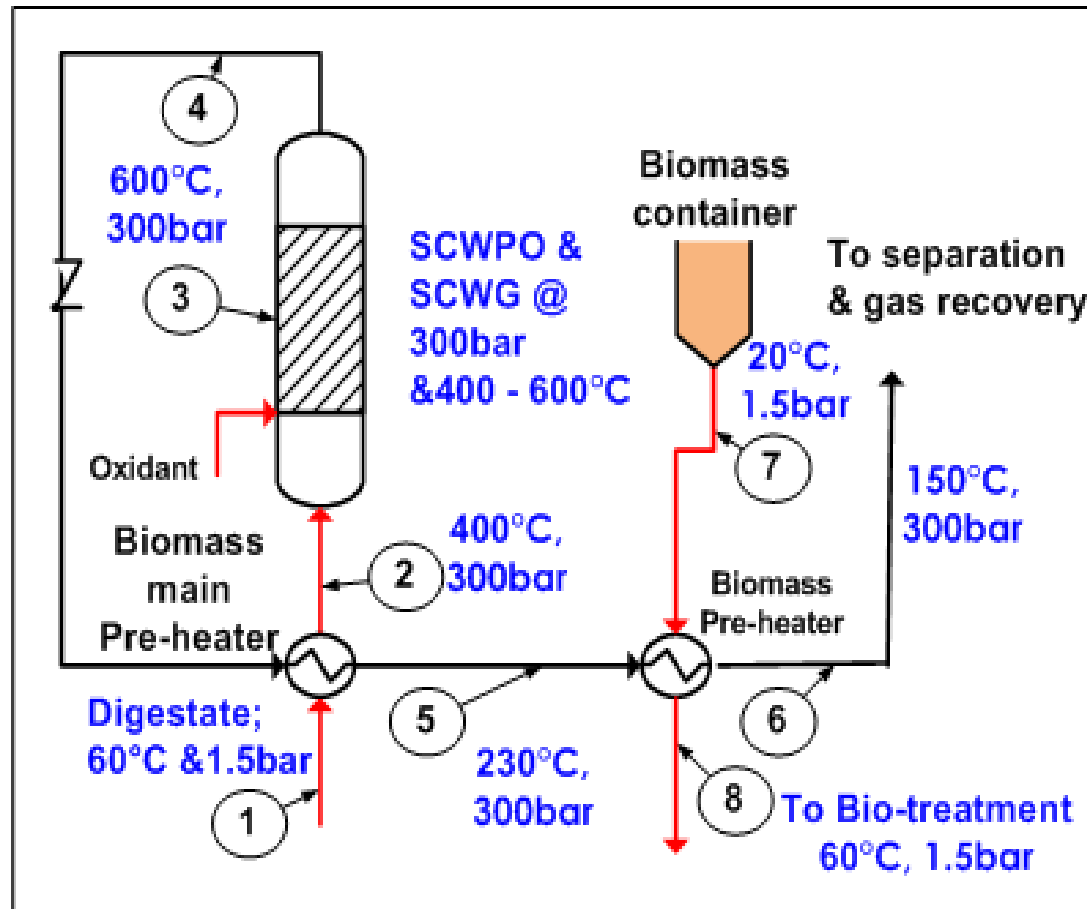
| Type                           | H <sub>2</sub> | CO  | CO <sub>2</sub> | CH <sub>4</sub> | N <sub>2</sub> | Tar              | Particles |
|--------------------------------|----------------|-----|-----------------|-----------------|----------------|------------------|-----------|
|                                |                |     |                 |                 |                | g/m <sup>3</sup> |           |
| Upstream/<br>Fxb./steam        | 30%            | 30% | 10%             | 10%             | 20%            | <b>100</b>       | >         |
| Downstream<br>/ Fxb./<br>steam | 50%            | 25% | 20%             | 10%             | n.d.           | <b>1</b>         | >         |
| Circ.<br>Fluidised             | 30%            | 25% | 25%             | 10%             | 10%            | <b>10</b>        | >>        |
| Circ.<br>Fluidised/<br>2-phase | 20%            | 20% | 10%             | 0%              | 41%            | low              | >>        |

# Gas Cleanup



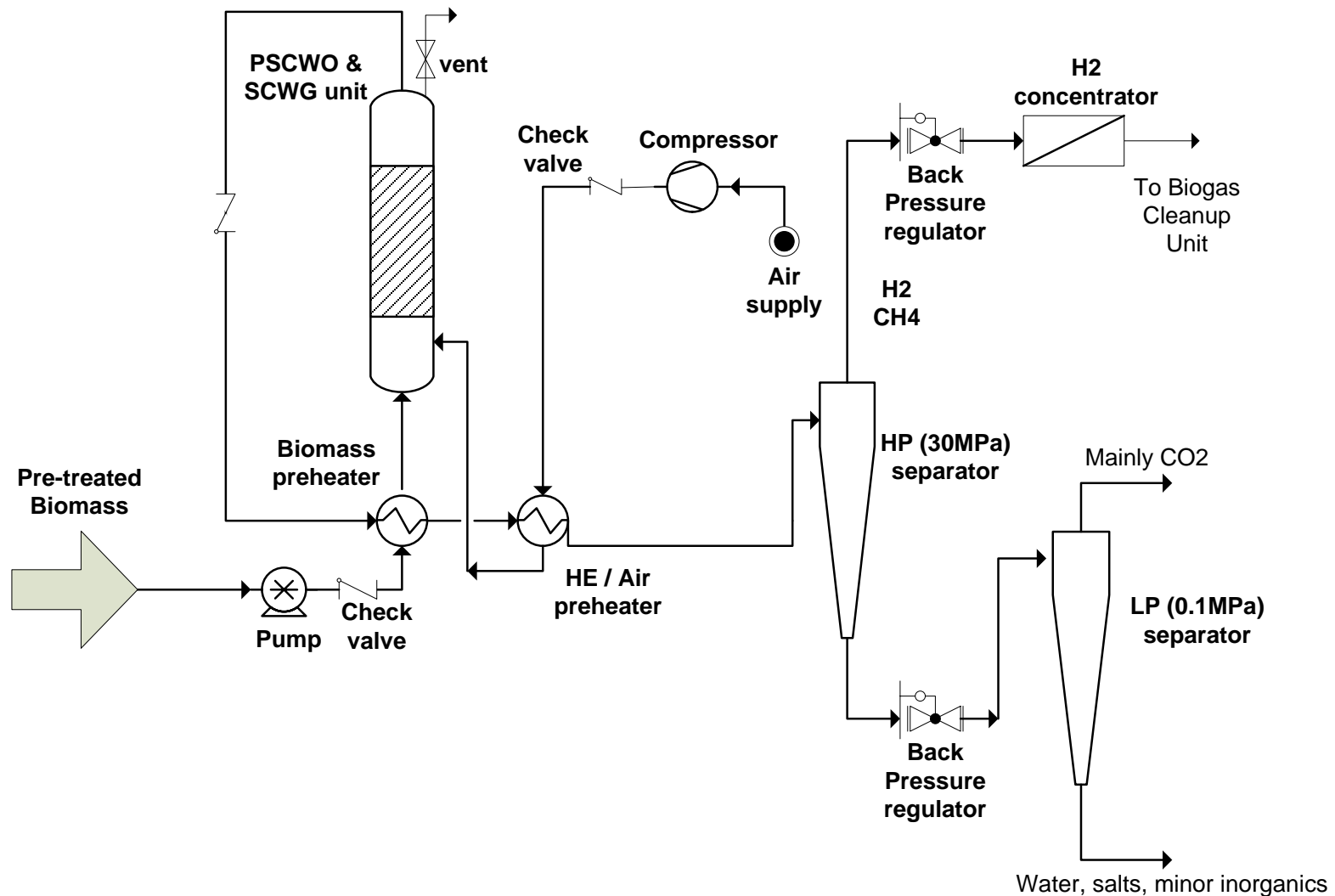
source: BioCleanGas

# Supercritical Water Gasification



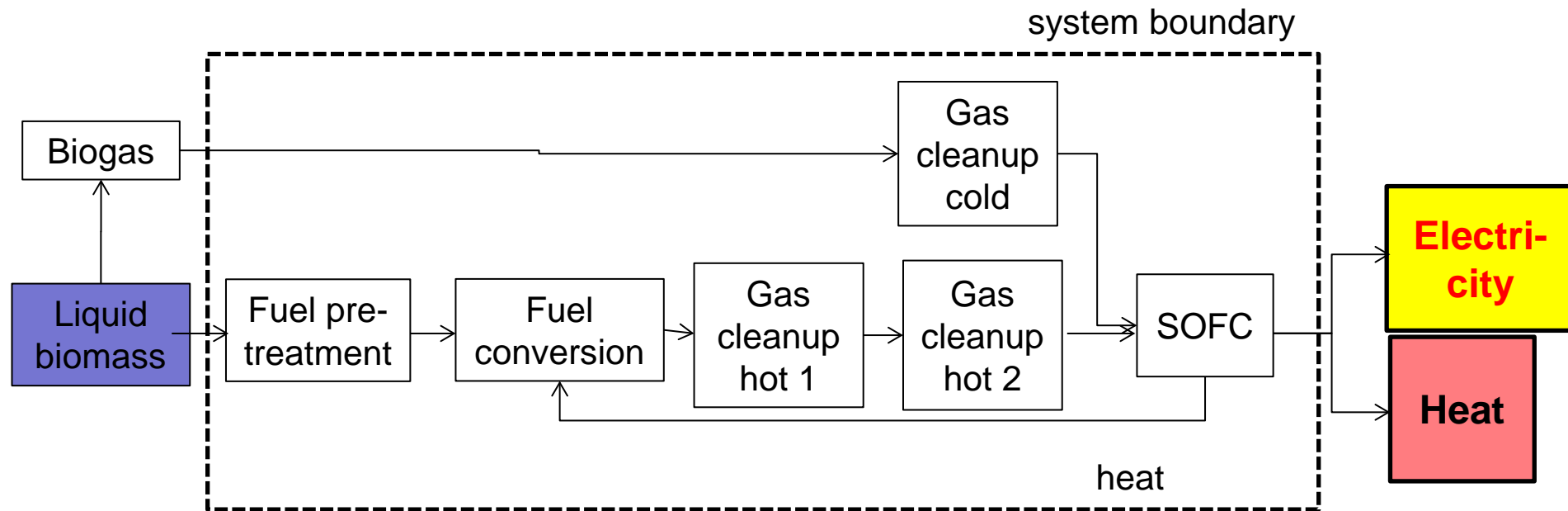
source: Bushra Al-Duri

# Supercritical Water Gasification (2)



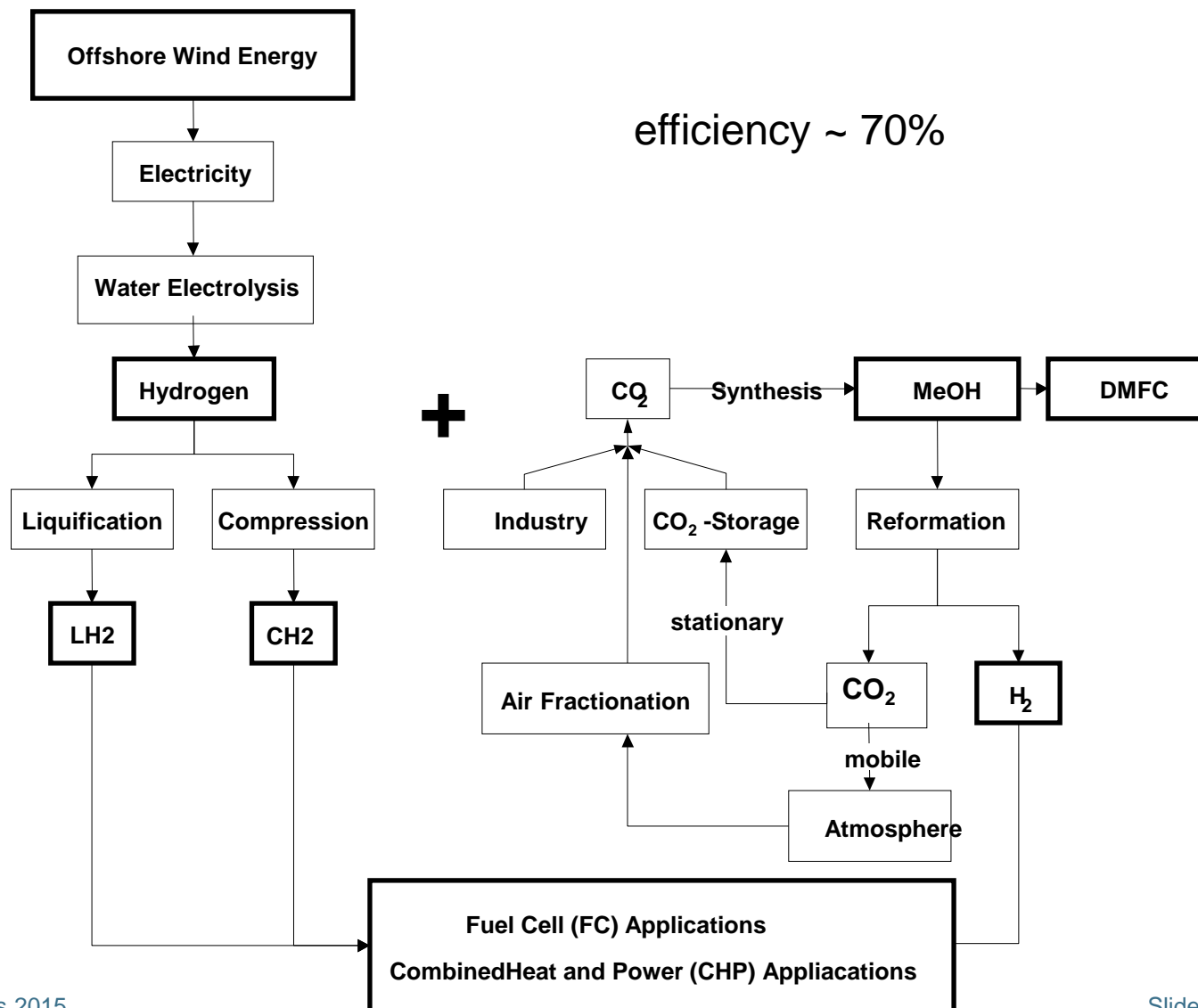
source: Bushra Al-Duri

# Hybrid Conversion System





# Liquid Product: Methanol Synthesis

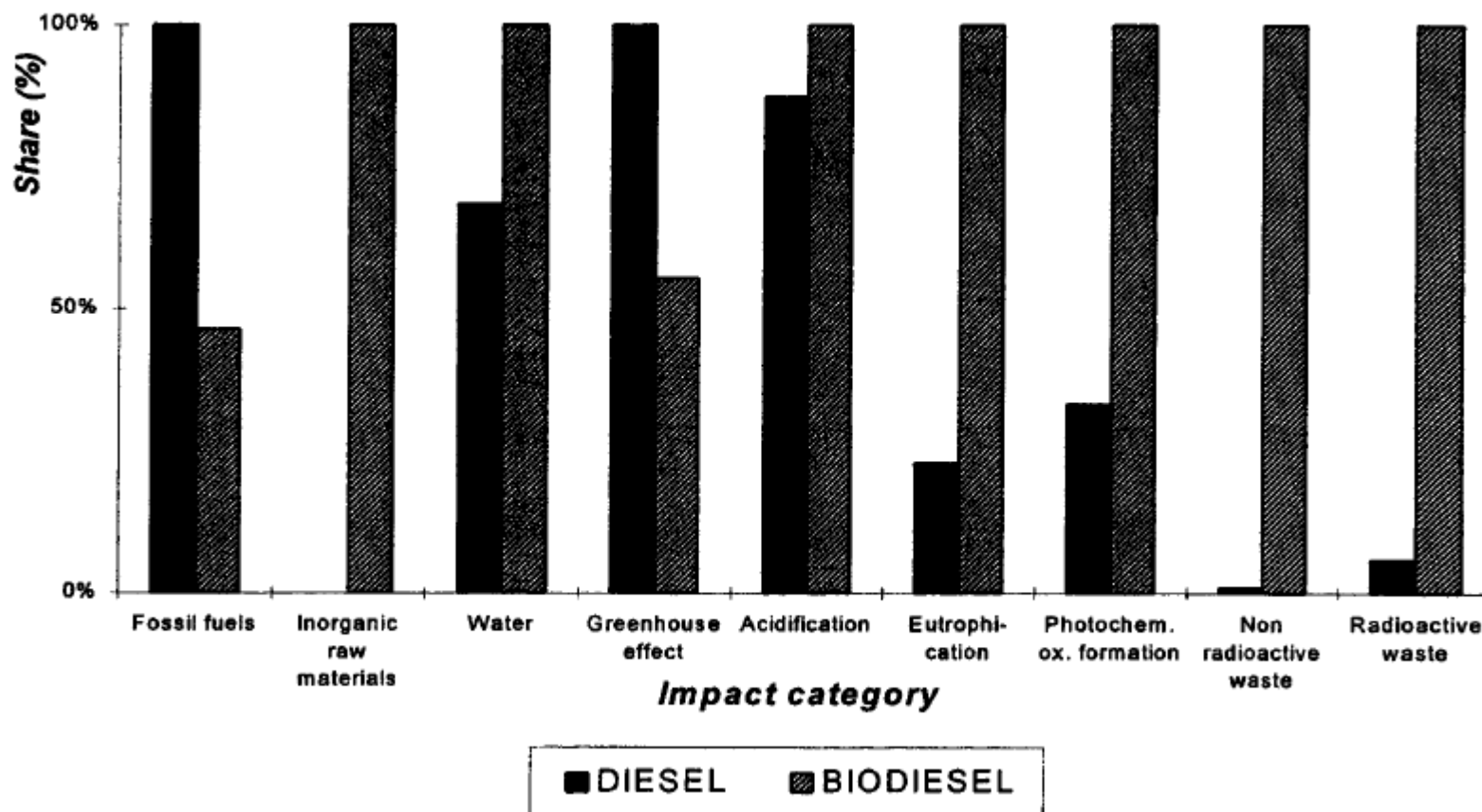




# Biomass Infrastructure

- 8 MW gasifier requires about 35 km radius collection of biomass
- trade-off between transport energy expense and energy yield
- energy density of biomass transport is questionable – rather transport product gas than the raw material

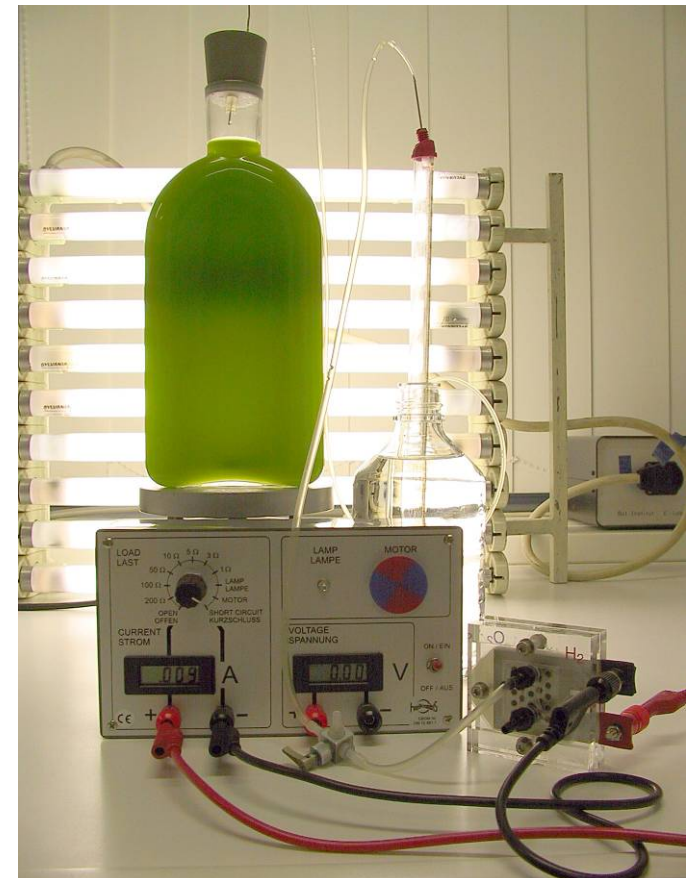
# Biomass Environmental Impact



## Food vs. Energy?

- is there an ethical dilemma?
- competition for resources:
  - not in Europe – agricultural over-production can be channelled into the energy market
- at a global scale:
  - potential competition has to be closely monitored – energy crops have to be grown as such and food crops not converted to energy crops – at the bottom line, though, the markets decide
- crop growing:
  - cultivation of energy crops releases  $\text{N}_2\text{O}_2$  – but so would food production

# Free Hydrogen Production: Algae and Bacteria



not quite for free: light and heat required, yield is limited

source: University of Bonn

# Summary

- a huge number of options exist to turn biomass into fuel gases suitable for SOFC
- this creates a high flexibility both of fuel supply and fuel use
- the product gases can be used for energy conversion, but also as chemical raw products, adding another degree of freedom
- issues of transport and distribution and scale of conversion need to be kept in mind
- a competition of food and energy use of biomass can be negated for the situation in Europe





**Thank you for your attention!**

**... and any questions?**

